

Client's Reference:	QG 01-2022 Qatargas Liquefied Gas Company Limited Majlis Al Taawon Street West Bay
	Doha, State of Qatar
For the attention of:	Mr. Michael Scott
Copy to:	Mr. Nishant Janbandhu
Report No. Report date Client	QA-0036-01-2022 13-Jan-22 Qatargas Liquefied Gas Company Limited
Ship Product	Arctic Voyager Liquefied Natural Gas
Port	Ras Laffan, Oatar
Loading commenced	12-Jan-22
Loading completed	13-Jan-22

We have pleasure in enclosing herewith, our report for the above referenced inspection.

The inspection was carried out according to the following reports:

Document Title		Pages
Contents Listing		One
Time Log		One
Inspection Checklist Page 1 of 2		One
Inspection Checklist Page 2 of 2		One
Field Data Report		One
LNG Analysis Report		One
Boil-Off Analysis Report		One
Certificate Of Quality		One
Certificate Of Quantity (Loading Calculations Report)		One
Quantity Delivered		One
LNG Quantity Report		One
Certificate Of Loading (Page 1 of 2)		One
Certificate Of Loading (Page 2 of 2)		One
	Total pages:	13 pages

Should you have any query, or require any additional information, please contact Mr. Abdul Yagdi at our Doha office (telephone number +97444123456).

For and on behalf of Global Survey Solutions Limited:

Abdul Yagdi

CONTENTS LISTING



Report No.	QA-0036-01-2022
Report date	13-Jan-22
Ship	Arctic Voyager
Product	Liquefied Natural Gas
Port	Ras Laffan, Qatar
Loading commenced	12-Jan-22
Loading completed	13-Jan-22

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TIME LOG

Time	Date	Operations
23:30	11-Jan-22	Vessel arrived at sea bouy
00:12	12-Jan-22	Vessel anchored
00:12	12-Jan-22	Notice of Readiness tendered
06:30	12-Jan-22	Free pratique granted
07:45	12-Jan-22	Pilot on board
08:12	12-Jan-22	Anchors aweigh
10:36	12-Jan-22	First line ashore
11:42	12-Jan-22	All fast
12:06	12-Jan-22	Gangway secured
12:12	12-Jan-22	Inspector at terminal
12:30	12-Jan-22	Inspector boarded vessel
12:42	12-Jan-22	Pre-loading survey conducted
12:54	12-Jan-22	Figures calculated and agreed with Chief Officer
13:18	12-Jan-22	Commenced connection of loading arms
13:30	12-Jan-22	Liquid / vapour arms connected
14:12	12-Jan-22	Cooling down of cargo commenced
15:12	12-Jan-22	Cooling down of cargo completed
15:24	12-Jan-22	ESD system tested
15:45	12-Jan-22	Loading commenced
16:05	12-Jan-22	2nd pump on
16:15	12-Jan-22	3rd pump on
16:24	12-Jan-22	4th pump on
16:30	12-Jan-22	5th pump on
16:42	12-Jan-22	6th pump on
16:54	12-Jan-22	7th pump on
17:00	12-Jan-22	8th pump on
17:12	12-Jan-22	9th pump on
17:30	12-Jan-22	10th pump on
17:45	12-Jan-22	Loading rate normalized
17:45	13-Jan-22	Started sampling, analysis of LNG
23:30	13-Jan-22	1st analysis of boil-off done
23:30	13-Jan-22	Loading completed
02:30	14-Jan-22	Last analysis of LNG done
02:42	14-Jan-22	Started heating of loading arms
02:45	14-Jan-22	Started measurements on board
03:30	14-Jan-22	Ship's measurements completed
04:15	14-Jan-22	Calculations of ship's quantities completed
05:24	14-Jan-22	Hoses disconnected
05:30	14-Jan-22	Figures obtained
06:00	14-Jan-22	Documents on board
07:30	14-Jan-22	Pilot on board for unberthing
07:45	14-Jan-22	Vessel started leaving berth
08:24	14-Jan-22	Vessel sailed
09:30	15-Jan-22	ETA at the next port



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INSPECTION CHECKLIST

Page 1 of 2

If an item listed below was completed in accordance with the procedures, check "yes" If not, check "no" and explain under the comment section. If an item is not applicable write "n.a." (not applicable) next

NOTE: A completed copy of this checklist should be included with the measurement report.

Before Loading

1	Was a key meeting held with vessel representative and shore			
	representative?	17.1.6.1	х	
2	Were all shorelines checked and shore tanks gauged?	17.1.6.2.1	х	
		17.1.6.2.2	n.a.	
3	Were temperatures taken from all shore tanks?	17.1.6.3	n.a.	
4	Was the temperature device checked prior to use?	17.1.11.3.1	n.a.	
		17.1.11.3.2	n.a.	
		17.111.3.3	n.a.	
5	Were all aut. tank gauging and temperature devices checked?	17.1.11.3.4	n.a.	
6	Were all shore tanks sampled?	17.1.6.4.1	n.a.	
7	Was an automatic sampler used?	17.1.6.4.2	х	
8	Was the inline sampler checked?	17.1.6.5	х	
9	Was the cromatograph calibrated prior to loading?	17.1.6.6.1	х	
10	Were draft, trim and list recorded?	17.1.6.6.2	х	
11	Were vessel completely deballasted?	17.1.6.6.3	n.a.	
12	Were vessel deck lines drained?	17.1.6.6.4	n.a.	
13	Were on-board quantity gauges taken?	17.1.6.6.5	х	
14	Were on-board quantity temperature taken?	17.1.6.6.6	х	
15	Were on board pressures taken?	17.1.6.6.7	х	
16	Were bunker quantities verified?	17.1.6.6.8	х	
17		17.1.6.6.9		
18		17.1.6.6.10		
19		17.1.6.6.11		
20		17.1.6.6.12		

During Loading

21	Were any difficulties encountered?	17.1.7.1		х	
22	Was line sample drawn?	17.1.7.2	х		
23		17.1.7.3			



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INSPECTION CHECKLIST

Page	2	of	2
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Item Number	Action	Section	Yes	No	No. of remark
	After Loading				<u> </u>
24 25 26	Were draft, trim, and list recorded? Were all vessel ullages, temperatures & pressure measurements recorded?	17.1.8.1 17.1.8.2 17.1.8.3 17.1.8.4	x x x n.a.		
27 28 29	Were temperatures taken in all vessel compartments? Were bunker quantities verified? Were vessel volumes recorded and calculated?	17.1.8.5 17.1.8.6 17.1.8.7 17.1.8.8	X X X X		
30 31 32 33 34 35 36 37 38 39 40 41 42	Were all closing tank gauges taken? Were tank samples taken? Were proper automatic sampling and samples mixing performed Were copies of analysis of samples taken obtained? Was qualitative testing performed according to directions furnished by interested parties? Was a time Log maintained? Were any Letter of Protest or Notices of Apparent Discrepancy issued during loading?	17.1.8.9 17.1.8.10 17.1.8.11 17.1.9.1 17.1.9.2 17.1.9.3 17.1.9.4 17.1.9.5 17.1.10.1 17.1.10.2 17.1.10.3 17.1.10.4 17.1.10.5 17.1.10.6	n.a. n.a. n.a. x x x x	x x	
No. 1 2 3 4 5 6 7 8 9 10 11 12 13 14	REMARKS:				



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FIELD DATA REPORT

MEASUREMENTS BEFORE LOADING

Date:	12-Jan-22	Time:	12:42		Trim: 0 m		List: 0.01°S	tbd	
Tank No.	Liquid Tempera- ture (°C)	Gas Tempera- ture (°C)	Recorded Level (m)	Trim + List Correction (m)	Temperature Correction (m)	Density Correctio n (m)	Total Correction (m)	Corrected Level (m)	Volume at calibration temperature (m ³)
1		23.63	0.021					0.021	0.000
2		23.95	0.019					0.019	0.000
3		24.08	0.020					0.020	0.000
4		24.52	0.019					0.019	0.000
5									
6									

Total volume before loading at calibration temperature of -160°C:

Thermal expansion factor for LNG volume: 1.00000

Total volume before loading at average temperature of °C: 0.000

Expansion ratio of gas to liquid	612.784
Average Temperature of LNG on board	٥C
Average Temperature of Gas on board	24.05 °C
Pressure	1,414 Mbar

MEASUREMENTS AFTER LOADING

Date: 14-Jan-22 Tir

2 Time: 03:30

Trim: -0.0499999999999 List: 0.01°Stbd

Volume at Liquid Gas Trim + List Temperature Density Total calibration Recorded Corrected Tank No. Temperat Temperat Correction Correction Correctio Correction temperature Level (m) Level (m) ure (°C) ure (°C) (m) n (m) (m) (m) (m^3) -159.64 -122.62 22.914 0.003 22.914 20,436.303 1 2 -159.93 -116.13 26.870 0.004 26.870 49,012.117 3 -159.94 -137.74 26.861 0.004 26.861 48,987.710 4 -159.94 -127.67 23.191 0.004 23.191 43,909.949 5 6

Total volume after loading at calibration temperature of -160°C: 162,346.079

Thermal expansion factor for LNG volume: 1.00000

Total volume after loading at average temperature of -159.86°C: 162,346.079

Expansion ratio of gas to liquid	612.784
Average Temperature of LNG on board	-159.86 °C
Average Temperature of Gas on board	-126.04 °C
Pressure	1,417 Mbar



Global Survey Solutions Ltd.

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LNG ANALYSIS REPORT

Analytical determination on vapour samples drawn by means of automatic sampler from shore line during discharge and analyzed in the laboratory of Messrs. QATARGAS S.A. by means of gas chromatographic equipment.

Sampler Global Survey Solutions Limited Date 14-Jan-22 Time

Components	Formula	Units	Method	Result
methane	CH4	mole %	GPA 2261-13	96.7000
ethane	C2H6	mole %	GPA 2261-13	2.4000
propane	C3H8	mole %	GPA 2261-13	0.5100
n-butane	C4H10	mole %	GPA 2261-13	0.1100
isobutane [2-methylpropane]	C4H10	mole %	GPA 2261-13	0.0900
n-pentane	C5H12	mole %	GPA 2261-13	
isopentane [2-methylbutane]	C5H12	mole %	GPA 2261-13	0.0200
n-hexane	C6H14	mole %	GPA 2261-13	
n-heptane	C7H16	mole %	GPA 2261-13	
ethylene [ethene]	C2H4	mole %	GPA 2261-13	
propylene [propene]	C3H6	mole %	GPA 2261-13	
1-butene [n-butylene]	C4H8	mole %	GPA 2261-13	
hydrogen sulfide [hydrogen sulphide]	H2S	mole %	GPA 2261-13	
nitrogen	N2	mole %	GPA 2261-13	0.1700
oxygen	02	mole %	GPA 2261-13	
carbon dioxide	CO2	mole %	GPA 2261-13	

Parameters	Units	Method	Result
Impurities			
Total sulphur	ppm	ASTM D6667	< 0.5
Mercaptans	ppm	BS ISO 19739:2004	< 0.1
Carbonyl Sulphide & Hydrogen Sulphide	ppm	BS ISO 19739:2004	< 0.1
Mercury	ppb	ASTM D6350	< 1
Hydrocarbon dewpoint (max)	^o C (between 1-80 bar)	ISO/TR 11150:2007	-45.2



Report No.QA-0036-01-2022Report date13-Jan-22ShipArctic VoyagerProductLiquefied Natural GasPortRas Laffan, QatarLoading commenced12-Jan-22Loading completed13-Jan-22

BOIL-OFF ANALYSIS REPORT

Analytical determination on vapour samples drawn by means of automatic sampler from shore line during discharge and analyzed in the laboratory of Messrs. QATARGAS S.A. by means of gas chromatographic equipment.

Sampler Global Survey Solutions Limited Date 13-Jan-22 Time 23:30

Components	Formula	Units	Method	Result
methane	CH4	mole %	GPA 2261-13	98.4839
ethane	C2H6	mole %	GPA 2261-13	0.1764
propane	C3H8	mole %	GPA 2261-13	0.0140
n-butane	C4H10	mole %	GPA 2261-13	0.0016
isobutane [2-methylpropane]	C4H10	mole %	GPA 2261-13	0.0018
n-pentane	C5H12	mole %	GPA 2261-13	0.0005
isopentane [2-methylbutane]	C5H12	mole %	GPA 2261-13	0.0010
n-hexane	C6H14	mole %	GPA 2261-13	
n-heptane	C7H16	mole %	GPA 2261-13	
ethylene [ethene]	C2H4	mole %	GPA 2261-13	
propylene [propene]	C3H6	mole %	GPA 2261-13	
1-butene [n-butylene]	C4H8	mole %	GPA 2261-13	
hydrogen sulfide [hydrogen sulphide]	H2S	mole %	GPA 2261-13	
nitrogen	N2	mole %	GPA 2261-13	1.3208
oxygen	02	mole %	GPA 2261-13	
carbon dioxide	CO2	mole %	GPA 2261-13	



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CERTIFICATE OF QUALITY

Total Net Quantity Delivered

3,651,375.58 MMBTU at 15°C 1,069,864,682.6 kW/hour

Average results of analysis at the laboratory of Enagas S.A., Huelva

Component	Formula	Mol %
methane	CH4	96.7000
ethane	C2H6	2.4000
propane	C3H8	0.5100
n-butane	C4H10	0.1100
isobutane [2-methylpropane]	C4H10	0.0900
n-pentane	C5H12	
isopentane [2-methylbutane]	C5H12	0.0200
n-hexane	C6H14	
n-heptane	C7H16	
ethylene [ethene]	C2H4	
propylene [propene]	C3H6	
1-butene [n-butylene]	C4H8	
hydrogen sulfide [hydrogen sulphide]	H2S	
nitrogen	N2	0.1700
oxygen	02	
carbon dioxide	CO2	
Total		100.0000

Temperature of the LNG

-159.86 °C

LNG-Properties	
Molar mass	16.6375 kg/kmol
Density of real gas at 15°C, 101.325 kPa	0.70516 kg/m3 (n)
Gross Calorific Value of the gas on volume basis at 15°C, 101.325 kPa	38,797.6 kJ/m3
Net Calorific Value of the gas on volume basis at 15°C, 101.325 kPa	38,881.2 kJ/m3
Expansion ratio of gas to LNG	612.784 m3 (N)/m3 LNG
LNG Density at -159.86°C	432.111 kg/m3
Gross Calorific Value by mass of LNG at 15°C	55,139 kJ/kg
Net Calorific Value by mass of LNG at 15°C	49,697 kJ/kg
Gross heating value of the LNG on volume basis at -159.86°C	23,826.168 gJ/m3
Ideal Gas Wobbe Index at 15°C	51,191.739 KJ/m3
Real Gas Wobbe Index at 15°C	51,257.446 KJ/m3

For and on behalf of Global Survey Solutions Limited:

Abdul Yagdi



Report No.
Report date
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Port
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Loading completed

QA-0036-01-2022 13-Jan-22 Arctic Voyager Liquefied Natural Gas Ras Laffan, Qatar 12-Jan-22 13-Jan-22

CERTIFICATE OF QUANTITY

LOADING CALCULATIONS REPORT

Specific Weight of LNG, kg/m ³	432.111
Gross Heating value of LNG on mass basis, MJ/kg	55.139
Density of real gas at , kg/m3	0.70516

Date:	12-Jan-22	14-Jan-22
Time:	12:42	03:30

Observed quantities

	Before	After	
	Observed LNG	Observed LNG	
Tank No.	Volume,	Volume,	
	m ³	m ³	
1	0.000	20,436.303	
2	0.000	49,012.117	
3	0.000	48,987.710	
4	0.000	43,909.949	
5			
6			

Total quantities

Total Volume, m3, at calibration temperature of -160°C	0.000	162,346.079
Average LNG temperature, °C		-159.86
Thermal expansion factor for LNG volume	1.00000	1.00000
Total Corrected LNG Volume, m3	0.000	162,346.079
Weight of LNG, Metric tons	0.000	70,151.527
Energy of LNG, TJ	0.000	3,868.085

Net quantities

	LNG Volume, m ³	LNG Weight, kg	LNG Energy, TJ
(+) Variation of quantity on board	162,346.079	70,151,527	3,868.085
(+) Own use by the ship	38.104	16,465	893.938
(-) Boil - Off	706.441	305,261	16.832
Net Loaded Quantity	161,677.742	69,862,731	4,745.191

For and on behalf of Global Survey Solutions Limited:

Abdul Yagdi



Report No. Report date Ship Product Port Loading commenced Loading completed QA-0036-01-2022 13-Jan-22 Arctic Voyager Liquefied Natural Gas Ras Laffan, Qatar 12-Jan-22 13-Jan-22

QUANTITY DELIVERED

(+) VARIATION OF QUANTITY ON BOARD Variation of Volume 162,346.079 m3 LNG Variation of Mass 70,151,527 kg Variation of Energy 3,666,236.695 MMBTU at 15°C 1,074,468,068.611 kW/hour 3,868,085.047 gJ Conversion Factor 0.947816981905 MMBTU/gJ (-) BOIL-OFF RETURNED 706.441 m3 LNG

(+) SHIP'S USE CONSUMPTION

305,261 kg 15,708.403 MMBTU at 15°C 4,603,679.1 kW/hour

25,237.823 m3 gas 38.104 m3 LNG 16,465 kg 847.290 MMBTU at 15°C 293.1 kW/hour

Total Quantity Delivered 3,651,375.58 MMBTU at 15°C 161,677.741 m3 LNG 1,069,864,682.56 kW/hour 99,073,586.906 m3 at 15°C, 101.325 kPa 69,862,731 kg

Report No. Report date Ship Product Port Loading commenced Loading completed QA-0036-01-2022 13-Jan-22 Arctic Voyager Liquefied Natural Gas Ras Laffan, Qatar 12-Jan-22 13-Jan-22

1. Composition Calculations

LNG QUANTITY REPORT

Component	Formula	Molar Fraction % (X _i)	Molar weight, kg/kmol, as per ISO 6578:2017, (Mi)	Molecular Mass (X _i *M _i)	Orthobaric Molar Volume, m3/kmol, at - 159.86°C as per NBS 1030-1980, (Vi)	Molar Fraction of Orthobaric Molar Volume, m3/kmol, at - 159.86°C as per NBS 1030-1980, (Vi * Vi)	Critical temperatu re, Tc,I, K by ISO 6578:201 7	Xi * Tc,i	Gross Calorific Value, kJ/mol at 15°C as per ISO 6976:2016, (GCVmol,i)	Σ(Xi*Mi*GCV mol,i)
methane	CH4	96.7000%	16.0420	15.512614	0.038167	0.0369077	190.555	184.26669	891.510	862.090170
ethane	C2H6	2.4000%	30.0690	0.721656	0.047954	0.0011509	305.420	7.33008	1562.140	37.491360
propane	C3H8	0.5100%	44.0960	0.224890	0.062509	0.0003188	369.820	1.88608	2221.100	11.327610
n-butane	C4H10	0.1100%	58.1220	0.063934	0.076889	0.0000846	425.180	0.46770	2879.760	3.167736
isobutane [2-methylpropane]	C4H10	0.0900%	58.1220	0.052310	0.078366	0.0000705	408.140	0.36733	2870.580	2.583522
n-pentane	C5H12									
isopentane [2-methylbutane]	C5H12	0.0200%	72.1490	0.014430	0.091737	0.0000183	460.430	0.09209	3531.680	0.706336
n-hexane	C6H14									
n-heptane	C7H16									
ethylene [ethene]	C2H4									
propylene [propene]	C3H6									
1-butene [n-butylene]	C4H8									
hydrogen sulfide [hydrogen sulphide]	H2S									
nitrogen	N2	0.1700%	28.0130	0.047622	0.047115	0.0000801	126.200	0.21454		
oxygen	02									
carbon dioxide	CO2									
Sum		100.0000%		16.6375	0.442738	0.0386309	194.62			917.367

2. Density calculation

K1 = 0.000128K2 = 0.000234

Liquid Temperature After, t°C = -159.86 °C Liquid Temperature After, K = T = t°C + 273.15 = 113.29K

Density (D), kg/m3 = $\frac{\Sigma(Xi * Mi)}{[\Sigma(Xi*Vi)] - [(K1+(K2-K1)*(Xn2/0.0425))*Xct]} = 432.111$

Remark: Density calculated as per Revised Klosek and McKinley (RKM) method, , Page 63, GIINGL 5.0, 2017

3. Gross Calorific Value

	GCVmass, mJ/kg =	Σ()	<u>(i*Mi*GCVmol,i)</u> = 55.139 mJ/kg (Σ(Xi*Mi)	(GCV)
GCVmass,Btu/SCF = 10000	00/(1055.056 * 836.614) * Σ(1.13285 * Σ(Xi*Mi*(Xi*Mi*(GCVmol,i) mJ/kg = GCVmol,i) mJ/kg = 1,039.3 BTU/S0	CF (GCV)
4. Quantity Delivered				
(-) Ship's arrival	0.000	m³	Vapour temp. before (Tv)	24.05 °C
(+) Ship's departure	162,346.079	m³	Abs. pressure before (P)	1,414 Milibars
(+) Own use by the ship	38.104	m³		
(-) Boil-Off	-706.441	m ³		
Net Ship loaded	161,677.742	m³		
	Q = (1/1055.056)*(V*D*GCV	/mass)	= 3,651,143.734 MMBtu	
5. Weight Delivered			= 69,862.731 Metric	Tons.
For and on behalf of Global S	Survey Solutions Limited:		Abdul Yagdi	Date: 13-Jan-22



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Ship	Arctic Voyager
Product	Liquefied Natural Gas
Port	Ras Laffan, Qatar
Loading commenced	12-Jan-22
Loading completed	13-Jan-22
Name of inspection con	Global Survey Solutions Limited
То	Qatargas Liquefied Gas Company Limited

CERTIFICATE OF LOADING

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1	IDENTIFICATION		
a)	Name of LNG Tanker	Arctic Voyager	
b)	Product	Liquefied Natural Gas	
c)	Loading commenced (date and time)	12-Jan-22	15:45
d)	Loading completed (date and time)	13-Jan-22	23:30
<u>2</u>	BASIC DATA		
a)	Volume loaded		161,677.741 m3
b)	Average temperature of LNG loaded		-159.86 °C
c)	Average temperature of LNG vapour in the LNG Tanker before loading		-126.04 °C
d)	Average absolute pressure of the LNG in the LNG Tanker before loading		1,417 millibar

e) LNG cargo composition

Loading

	Components by GPA 2261-13		Formula	Mole Percent
	methane		CH4	96.7000
	ethane		C2H6	2.4000
	propane		C3H8	0.5100
	n-butane		C4H10	0.1100
	isobutane [2-methylpropane]		C4H10	0.0900
	n-pentane		C5H12	
	isopentane [2-methylbutane]		C5H12	0.0200
	n-hexane		C6H14	
	n-heptane		C7H16	
	ethylene [ethene]		C2H4	
	propylene [propene]		C3H6	
	1-butene [n-butylene]		C4H8	
	hydrogen sulfide [hydrogen sulphide]		H2S	
	nitrogen		N2	0.1700
	oxygen		02	
	carbon dioxide		CO2	
f)	Parameters	Units	Method	Result
	Impurities			
	Total sulphur	ppm	ASTM D6667	< 0.5
	Mercaptans	ppm	BS ISO 19739:2004	< 0.1
	Carbonyl Sulphide & Hydrogen Sulphide	ppm	BS ISO 19739:2004	< 0.1
	Mercury	ppb	ASTM D6350	< 1
	Hydrocarbon dewpoint (max)	°C (between 1-80 bar)	ISO/TR 11150:2007	-45.2
g)				



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CERTIFICATE OF LOADING

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3. RESULTS

- a) Wobbe index of ideal gas
- b) Wobbe index of real gas
- c) LNG Density
- d) Gross Calorific Value by mass of LNG at 15°C
- e) Net Calorific Value by mass of LNG at 15°C
- f) Real Gas Gross Calorific Value at 15/15°C as per ISO 6976:2016
- g) Ideal Gas Net Calorific Value at 15/15°C as per ISO 6976:2016
- h) Real Gas Net Calorific Value at 15/15°C as per ISO 6976:2016
- j) Quantity of LNG vapour returned to LNG terminal during loading

4.- QUANTITY LOADED

51,191.739 KJ/m3 at 15°C, 101.325 kPa 51,257.446 KJ/m3 at 15°C, 101.325 kPa 432.111 kg/m3 55.139 MJ/kg calculated from GCV mola 49.697 MJ/kg calculated from NCV mola 38.881 MJ/m3 34.969 MJ/m3 35.044 MJ/m3 16,573,245.249 MJ at 15°C

1,069,864,682.6 kW/hour 3,651,375.58 MMBTU at 15°C 99,073,586.906 m3 at 15°C, 101.325 kPa

5.- CERTIFICATE OF LOADING

We hereby certify that according to the tests and measurements on loading, the LNG to be off-loaded at the Receiving Facilities should conform to certification on unloading set out in Clause 5.1. (b) of the SPA